

P21.7 (a) $PV = Nk_B T$: $N = \frac{PV}{k_B T} = \frac{1.013 \times 10^5 \text{ Pa} \left[\frac{4}{3} \pi (0.150 \text{ m})^3 \right]}{(1.38 \times 10^{-23} \text{ J/K})(293 \text{ K})} = \boxed{3.54 \times 10^{23} \text{ atoms}}$

(b) $\bar{K} = \frac{3}{2} k_B T = \frac{3}{2} (1.38 \times 10^{-23} \text{ J/K})(293 \text{ K}) = \boxed{6.07 \times 10^{-21} \text{ J}}$

(c) For helium, the atomic mass is $m = \frac{4.00 \text{ g/mol}}{6.02 \times 10^{23} \text{ molecules/mol}} = 6.64 \times 10^{-24} \text{ g/molecule}$
 $m = 6.64 \times 10^{-27} \text{ kg/molecule}$

$\frac{1}{2} m \overline{v^2} = \frac{3}{2} k_B T$: $\therefore v_{\text{rms}} = \sqrt{\frac{3k_B T}{m}} = \boxed{1.35 \text{ km/s}}$

P21.9 (a) $\bar{K} = \frac{3}{2} k_B T = \frac{3}{2} (1.38 \times 10^{-23} \text{ J/K})(423 \text{ K}) = \boxed{8.76 \times 10^{-21} \text{ J}}$

(b) $\bar{K} = \frac{1}{2} m v_{\text{rms}}^2 = 8.76 \times 10^{-21} \text{ J}$

so

$$v_{\text{rms}} = \sqrt{\frac{1.75 \times 10^{-20} \text{ J}}{m}} \quad (1)$$

For helium,

$$m = \frac{4.00 \text{ g/mol}}{6.02 \times 10^{23} \text{ molecules/mol}} = 6.64 \times 10^{-24} \text{ g/molecule}$$

$$m = 6.64 \times 10^{-27} \text{ kg/molecule}$$

Similarly for argon,

$$m = \frac{39.9 \text{ g/mol}}{6.02 \times 10^{23} \text{ molecules/mol}} = 6.63 \times 10^{-23} \text{ g/molecule}$$

$$m = 6.63 \times 10^{-26} \text{ kg/molecule}$$

Substituting in (1) above,

we find for helium,

$$v_{\text{rms}} = \boxed{1.62 \text{ km/s}}$$

and for argon,

$$v_{\text{rms}} = \boxed{514 \text{ m/s}}$$

P21.13 We use the tabulated values for C_p and C_v

(a) $Q = nC_p \Delta T = 1.00 \text{ mol}(28.8 \text{ J/mol} \cdot \text{K})(420 - 300) \text{ K} = \boxed{3.46 \text{ kJ}}$

(b) $\Delta E_{\text{int}} = nC_v \Delta T = 1.00 \text{ mol}(20.4 \text{ J/mol} \cdot \text{K})(120 \text{ K}) = \boxed{2.45 \text{ kJ}}$

(c) $W = -Q + \Delta E_{\text{int}} = -3.46 \text{ kJ} + 2.45 \text{ kJ} = \boxed{-1.01 \text{ kJ}}$

P21.21In the isovolumetric process $A \rightarrow B$, $W = 0$ and $Q = nC_V\Delta T = 500 \text{ J}$

$$500 \text{ J} = n \left(\frac{3R}{2} \right) (T_B - T_A) \text{ or } T_B = T_A + \frac{2(500 \text{ J})}{3nR}$$

$$T_B = 300 \text{ K} + \frac{2(500 \text{ J})}{3(1.00 \text{ mol})(8.314 \text{ J/mol} \cdot \text{K})} = 340 \text{ K}$$

In the isobaric process $B \rightarrow C$,

$$Q = nC_P\Delta T = \frac{5nR}{2}(T_C - T_B) = -500 \text{ J}.$$

Thus,

$$(a) \quad T_C = T_B - \frac{2(500 \text{ J})}{5nR} = 340 \text{ K} - \frac{1000 \text{ J}}{5(1.00 \text{ mol})(8.314 \text{ J/mol} \cdot \text{K})} = \boxed{316 \text{ K}}$$

(b) The work done on the gas during the isobaric process is

$$W_{BC} = -P_B\Delta V = -nR(T_C - T_B) = -(1.00 \text{ mol})(8.314 \text{ J/mol} \cdot \text{K})(316 \text{ K} - 340 \text{ K})$$

$$\text{or } W_{BC} = +200 \text{ J}$$

The work done on the gas in the isovolumetric process is zero, so in total

$$W_{\text{on gas}} = \boxed{+200 \text{ J}}.$$

P21.25

$$(a) \quad P_i V_i^\gamma = P_f V_f^\gamma$$

$$P_f = P_i \left(\frac{V_i}{V_f} \right)^\gamma = 5.00 \text{ atm} \left(\frac{12.0}{30.0} \right)^{1.40} = \boxed{1.39 \text{ atm}}$$

$$(b) \quad T_i = \frac{P_i V_i}{nR} = \frac{5.00(1.013 \times 10^5 \text{ Pa})(12.0 \times 10^{-3} \text{ m}^3)}{2.00 \text{ mol}(8.314 \text{ J/mol} \cdot \text{K})} = \boxed{365 \text{ K}}$$

$$T_f = \frac{P_f V_f}{nR} = \frac{1.39(1.013 \times 10^5 \text{ Pa})(30.0 \times 10^{-3} \text{ m}^3)}{2.00 \text{ mol}(8.314 \text{ J/mol} \cdot \text{K})} = \boxed{253 \text{ K}}$$

(c) The process is adiabatic: $\boxed{Q = 0}$

$$\gamma = 1.40 = \frac{C_P}{C_V} = \frac{R + C_V}{C_V}, \quad C_V = \frac{5}{2}R$$

$$\Delta E_{\text{int}} = nC_V\Delta T = 2.00 \text{ mol} \left(\frac{5}{2}(8.314 \text{ J/mol} \cdot \text{K}) \right) (253 \text{ K} - 365 \text{ K}) = \boxed{-4.66 \text{ kJ}}$$

$$W = \Delta E_{\text{int}} - Q = -4.66 \text{ kJ} - 0 = \boxed{-4.66 \text{ kJ}}$$

P22.6

The heat to melt 15.0 g of Hg is

$$|Q_c| = mL_f = (15 \times 10^{-3} \text{ kg})(1.18 \times 10^4 \text{ J/kg}) = 177 \text{ J}$$

The energy absorbed to freeze 1.00 g of aluminum is

$$|Q_h| = mL_f = (10^{-3} \text{ kg})(3.97 \times 10^5 \text{ J/kg}) = 397 \text{ J}$$

and the work output is

$$W_{\text{eng}} = |Q_h| - |Q_c| = 220 \text{ J}$$

$$e = \frac{W_{\text{eng}}}{|Q_h|} = \frac{220 \text{ J}}{397 \text{ J}} = 0.554, \text{ or } \boxed{55.4\%}$$

The theoretical (Carnot) efficiency is

$$\frac{T_h - T_c}{T_h} = \frac{933 \text{ K} - 243.1 \text{ K}}{933 \text{ K}} = 0.749 = 74.9\%$$

P22.7

$$\text{COP}(\text{refrigerator}) = \frac{Q_c}{W}$$

(a) If $Q_c = 120 \text{ J}$ and $\text{COP} = 5.00$, then $\boxed{W = 24.0 \text{ J}}$

(b) Heat expelled = Heat removed + Work done.

$$Q_h = Q_c + W = 120 \text{ J} + 24 \text{ J} = \boxed{144 \text{ J}}$$

P22.11

$$T_c = 703 \text{ K} \quad T_h = 2143 \text{ K}$$

(a) $e_c = \frac{\Delta T}{T_h} = \frac{1440}{2143} = \boxed{67.2\%}$

(b) $|Q_h| = 1.40 \times 10^5 \text{ J}$, $W_{\text{eng}} = 0.420|Q_h|$
 $\dot{W} = \frac{W_{\text{eng}}}{\Delta t} = \frac{5.88 \times 10^4 \text{ J}}{1 \text{ s}} = \boxed{58.8 \text{ kW}}$

P22.13

Isothermal expansion at $T_h = 523 \text{ K}$ Isothermal compression at $T_c = 323 \text{ K}$

Gas absorbs 1 200 J during expansion.

(a) $|Q_c| = |Q_h| \left(\frac{T_c}{T_h} \right) = 1200 \text{ J} \left(\frac{323}{523} \right) = \boxed{741 \text{ J}}$

(b) $W_{\text{eng}} = |Q_h| - |Q_c| = (1200 - 741) \text{ J} = \boxed{459 \text{ J}}$

P22.17

(a) In an adiabatic process, $P_f V_f^\gamma = P_i V_i^\gamma$. Also, $\left(\frac{P_f V_f}{T_f}\right)^\gamma = \left(\frac{P_i V_i}{T_i}\right)^\gamma$.

Dividing the second equation by the first yields $T_f = T_i \left(\frac{P_f}{P_i}\right)^{(\gamma-1)/\gamma}$.

Since $\gamma = \frac{5}{3}$ for Argon, $\frac{\gamma-1}{\gamma} = \frac{2}{5} = 0.400$ and we have

$$T_f = (1073 \text{ K}) \left(\frac{300 \times 10^3 \text{ Pa}}{1.50 \times 10^6 \text{ Pa}} \right)^{0.400} = \boxed{564 \text{ K}}.$$

(b) $\Delta E_{\text{int}} = nC_V \Delta T = Q - W_{\text{eng}} = 0 - W_{\text{eng}}$, so $W_{\text{eng}} = -nC_V \Delta T$,

and the power output is

$$\begin{aligned} \mathcal{P} &= \frac{W_{\text{eng}}}{t} = \frac{-nC_V \Delta T}{t} \text{ or} \\ &= \frac{(-80.0 \text{ kg}) \left(\frac{1.00 \text{ mol}}{0.0399 \text{ kg}} \right) \left(\frac{3}{2} \right) (8.314 \text{ J/mol} \cdot \text{K}) (564 - 1073) \text{ K}}{60.0 \text{ s}} \\ \mathcal{P} &= 2.12 \times 10^5 \text{ W} = \boxed{212 \text{ kW}} \end{aligned}$$

(c) $e_C = 1 - \frac{T_c}{T_h} = 1 - \frac{564 \text{ K}}{1073 \text{ K}} = 0.475 \text{ or } \boxed{47.5\%}$

Quick Quiz 22.3.

If COP is 4, you need to do 0.25 of Work to transfer heat amount of 1.

$$\text{COP} \equiv \frac{Q}{W} \begin{array}{l} \leftarrow \text{Heat from cold to hot} \\ \text{or from hot to cold} \\ \nwarrow \text{Work done by engine} \end{array}$$